



Introduction to Chemical Kinetics for Combustion

PART II

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Outline

- ❑ What drives combustion?
- ❑ Temperature dependency of chemical kinetic pathways (aka low T chemistry)
- ❑ Chemical kinetic model reduction and stiffness removal
- ❑ Extension to CFD: is detailed chemistry always the answer?

What drives combustion?

It is the radicals, stupid!



What drives reaction progress in combustion?

Reaction progress driven mostly by **radicals**

- ❑ The electronic configuration of an atom determines **its valence**, that is, the number of electrons in the outermost shell (highest energy levels) able to form bonds.
- ❑ A radical is formed when one of the valence electrons is not paired.
- ❑ Radicals are highly reactive and tend to react with other species to reach the more stable paired-electron configuration



Radicals drive reaction progress in combustion

Radical balance is the most important aspect

□ 4 types of reactions:

□ **Initiation** reactions – Stable molecules creating radicals

What are the initiation reactions in the heptane/air case from part I?

#P 78. N-C7H16 REACTIONS

n196: N-C7H16	-> p-C4H9 + n-C3H7	{ a = 3.160E+16 n = 0 E = 339.2 }
n197: N-C7H16 + H	-> 1-C7H15 + H2	{ a = 7.300E+07 n = 2 E = 32.2 }
n198: N-C7H16 + H	-> 2-C7H15 + H2	{ a = 3.500E+07 n = 2 E = 20.9 }
n201: N-C7H16 + OH	-> 1-C7H15 + H2O	{ a = 10.560E+09 n = 1.1 E = 7.6 }
n202: N-C7H16 + OH	-> 2-C7H15 + H2O	{ a = 5.200E+09 n = 1.3 E = 2.9 }
n209: N-C7H16 + H2O2	-> 1-C7H15 + H2O2	{ a = 1.790E+13 n = 0 E = 81.2 }
n210: N-C7H16 + H2O2	-> 2-C7H15 + H2O2	{ a = 13.400E+12 n = 0 E = 71.2 }
n217: N-C7H16 + O2	-> 1-C7H15 + HO2	{ a = 5.500E+13 n = 0 E = 205.2 }
n218: N-C7H16 + O2	-> 2-C7H15 + HO2	{ a = 8.000E+13 n = 0 E = 199.3 }



Radicals drive reaction progress in combustion

Radical balance is the most important aspect

□ 4 types of reactions:

□ **Initiation** reactions – Stable molecules creating radicals

□ **Chain-branching reactions** – more radicals in reactants than in products
Example

□ **Chain-Propagating** reactions – Same number of radicals on both sides
Example

□ **Chain-breaking/terminating** reactions – Fewer radicals in reactants than in products
Example



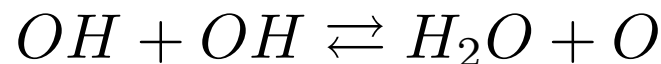
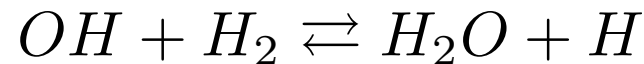
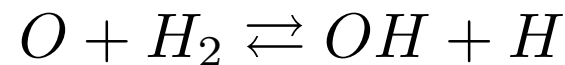
Radicals drive reaction progress in combustion

❑ **Most important** radicals for combustion:

and in specific conditions,

❑ O is different from the others:

❑ They play similar roles in the kinetics due to fast shuffling reactions





Radicals drive reaction progress in combustion

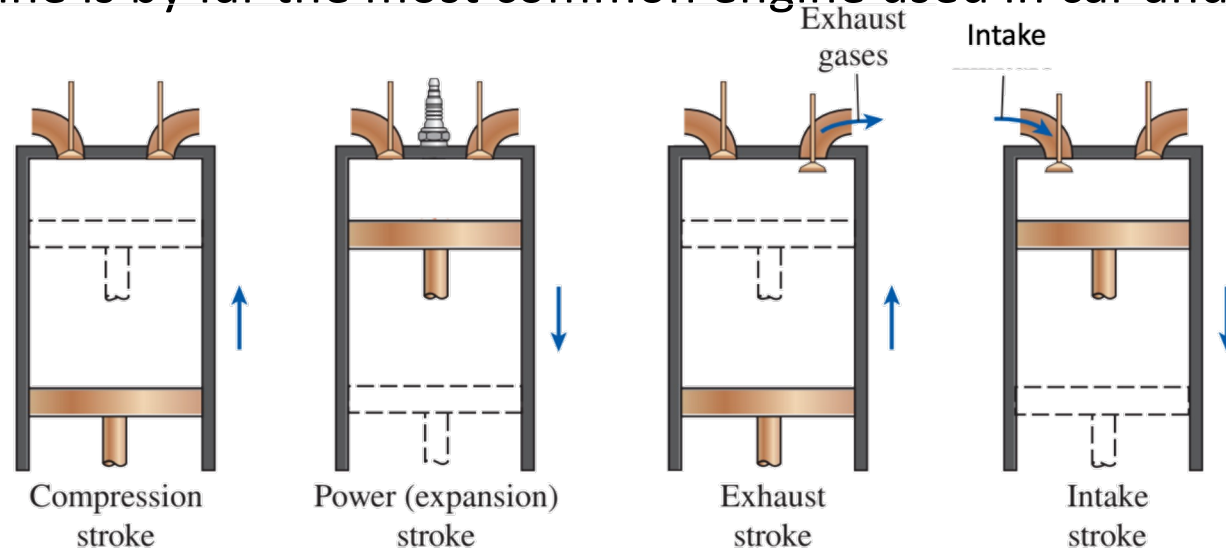
- ❑ Most important **chain-branching** reaction
- ❑ Very significant reaction for **chain-breaking**:

Chemical kinetics pathways are strong function of the temperature

Quick overview of low temperature chemistry

Application: Internal combustion engines

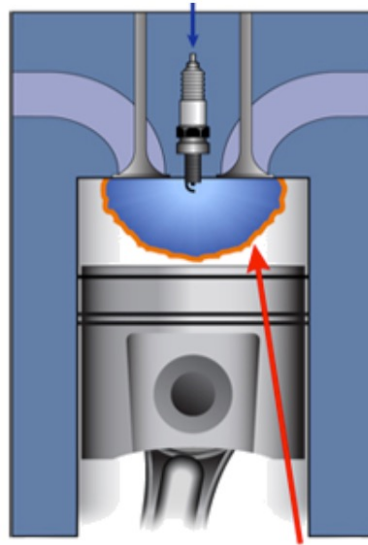
- 4-stroke engine is by far the most common engine used in car and trucks



Spark-ignition (gasoline)

- Pre-vaporized fuel and air during intake
- Timing of combustion through spark
- Premixed flame propagation

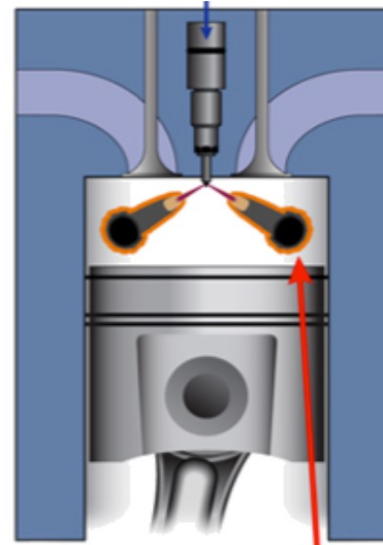
Low emissions



Compression-ignition (diesel)

- Only air during intake
- Timing of combustion through fuel injection
- Autoignition and mixed mode of combustion

High emissions



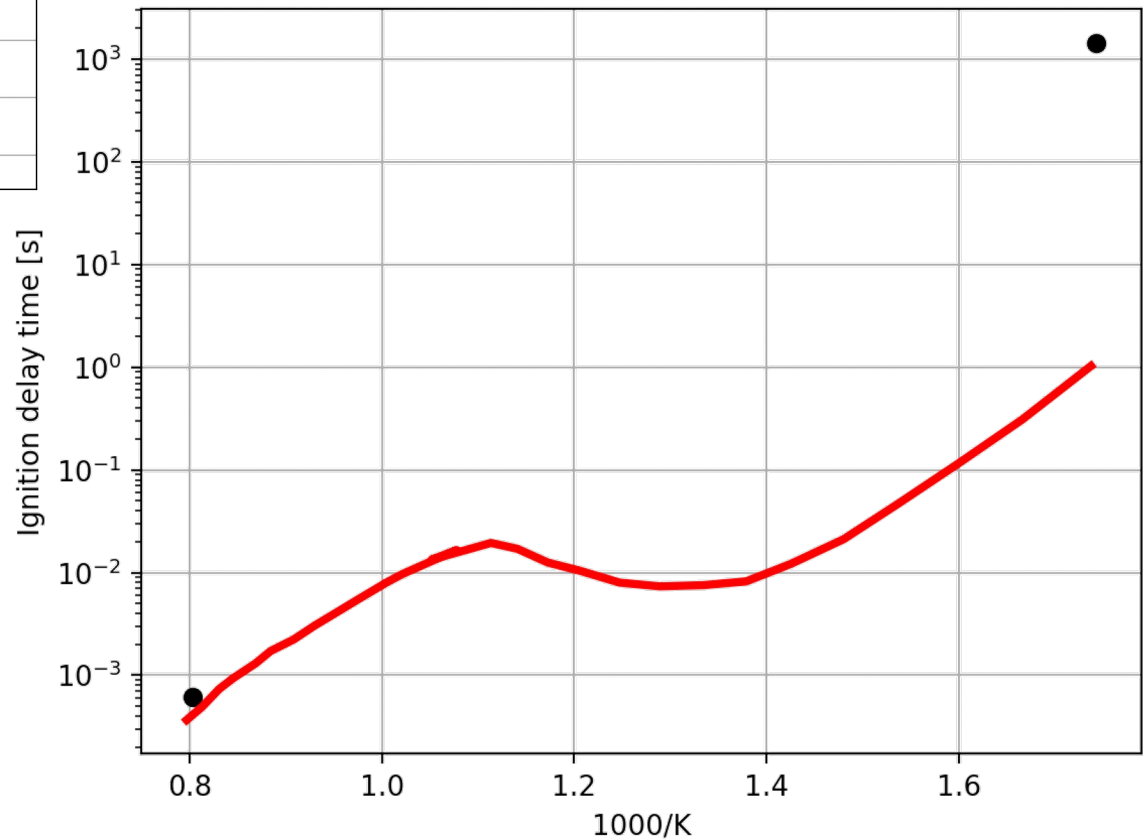
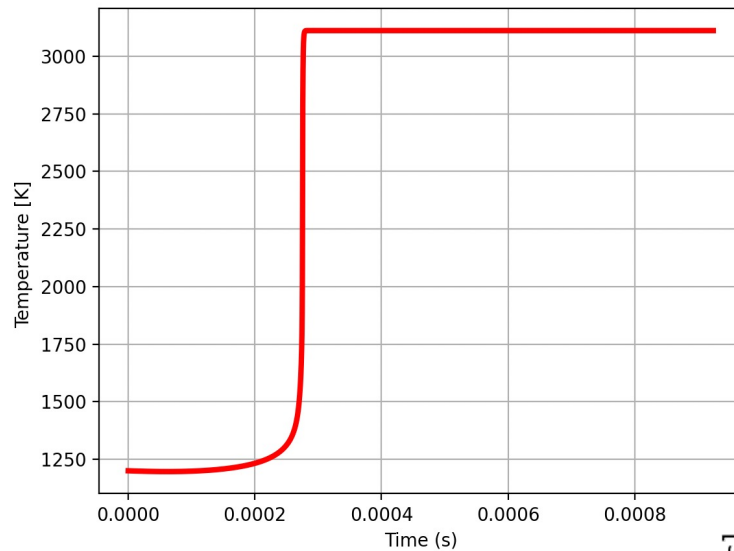
Application: Internal combustion engines

- ❑ Thermal efficiency related to compression ratio
- ❑ Typical compression ratios:
- ❑ What happens if you put gasoline into a pure ethanol engine (both SI)?
 - ❑ Vaporization is not the same, issue with cold start
 - ❑ Global reaction VERY different, you would be injecting way too much gasoline and burning very rich
 - ❑ Flame speeds not the same: ignition time advance (when spark plug goes off) would be off
 - ❑ Spark plugs, oxygen sensors, catalytic converters would be in trouble
 - ❑ Octane number is very different: high risk of knocking! Fuel/air mixture auto-ignites before flame gets to it, creating undesirable pressure peaks



Ignition delay time and its temperature dependency

Temperature profile for heptane/air





Heptane auto-ignition at high temperature

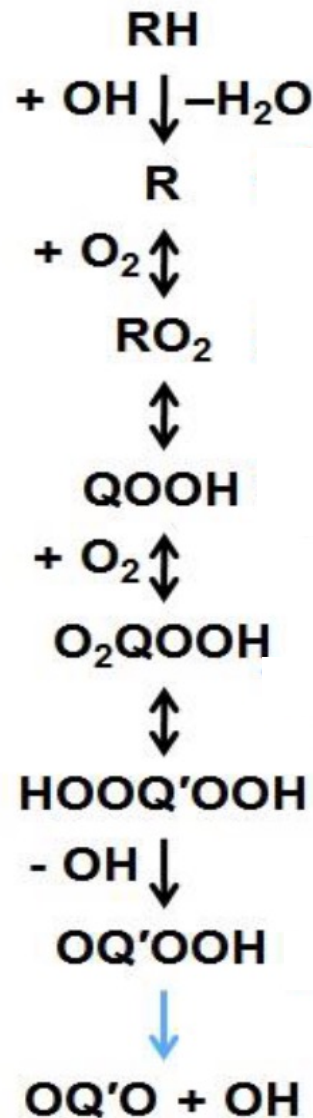
- ❑ Initiation reactions
- ❑ As soon as there is some H in the system, favorite chain-branching reaction starts cranking radicals
- ❑ Fuel radicals are short-lived: most favored reaction involves breaking the chain into small pieces
- ❑ Once the HC fragments are small enough, oxidation starts, creating C-O bonds, removing hydrogen
- ❑ At the end, CO is fully oxidized to CO₂ nearly exclusively through

At high temperature, fuel quickly breaks down to small fragments and C-O bonds are formed on C1-C2 species

- **Most fuels behave the same**
- **Very good understanding of the chemistry and associated rates**

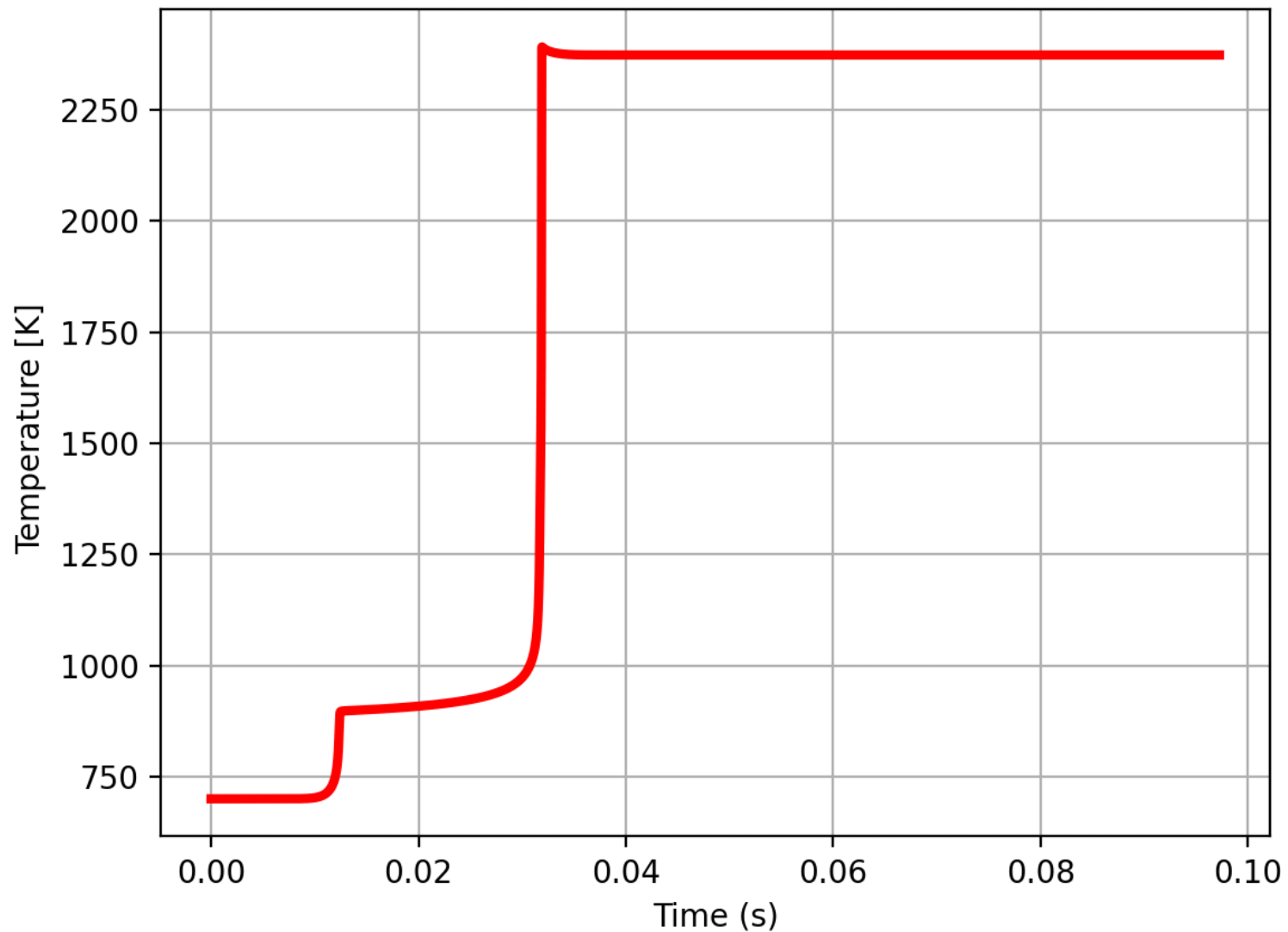
Heptane auto-ignition at low-temperature

- Initiation starts the same. However, unimolecular breakdown of the fuel molecule is not favored anymore: fuel radical is long-lived

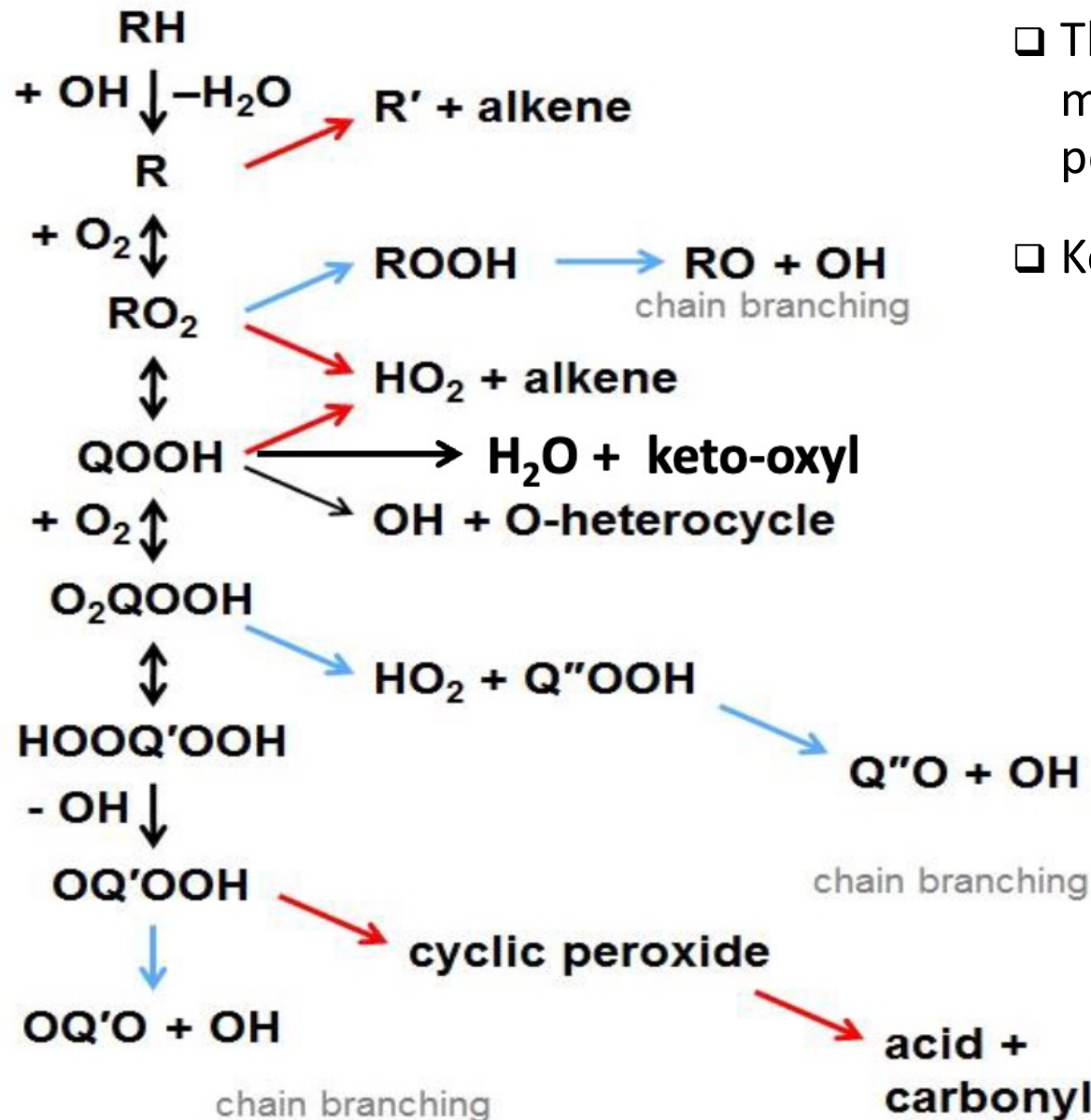


Heptane auto-ignition at low-temperature

- Temperature profile is quite specific



Heptane auto-ignition at low-temperature

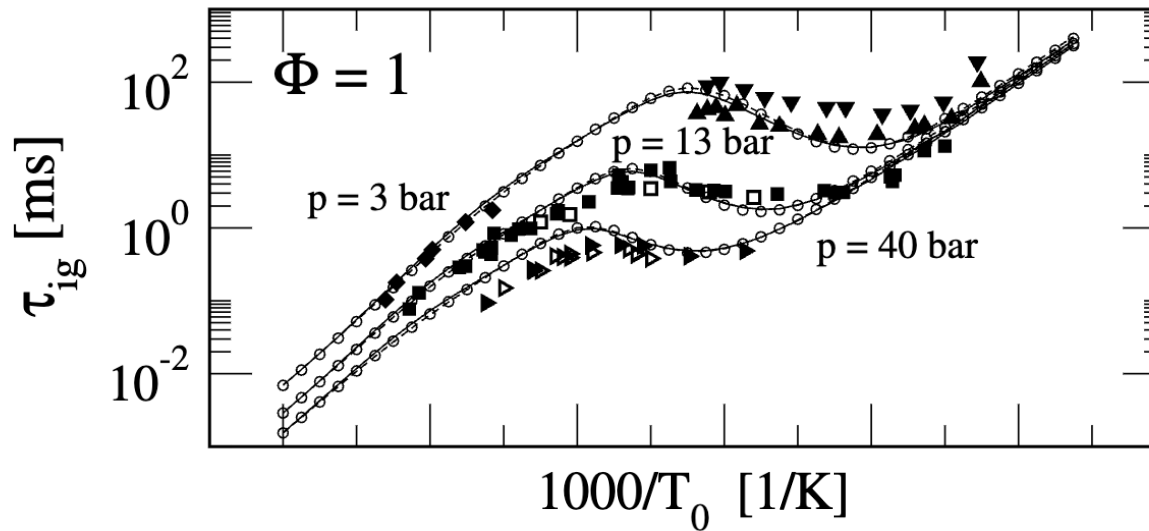


□ The actual chemistry is much more complicated, with many potential side channels

□ Key challenge:

Overall, reasonably well understood

Heptane auto-ignition at medium temperatures

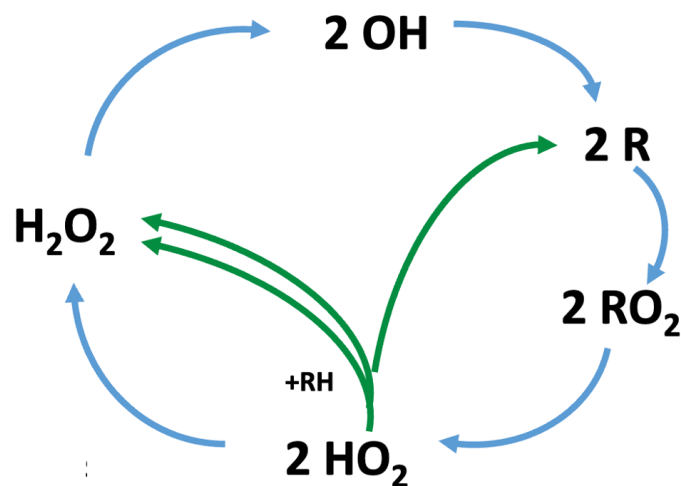


- In an intermediate range of temperature, there is a **kinetically favored** kinetic pathway that is
 - More efficient at igniting than the high temperature pathway (unimolecular decompositions need lots of energy to proceed)
 - Less efficient at igniting than the low temperature pathway (OH is getting replaced by some other radical)



Heptane auto-ignition at medium temperatures

- At medium T, the fuel radical is very slow at breaking down
 - O_2 has its chance! But when R and O_2 combine, they do not result in RO_2
- In addition, our favorite chain branching reaction gets side lined
- HO_2 still creates a chain-branching cycle



**Moderately well
understood, less so
than the other regimes**

When detailed chemistry is too detailed

Sometimes it is...

Numerical simulations

- ❑ **What we want:** couple kinetics info with real-world combustion, which is virtually always turbulent
- ❑ **What we can do** with detailed chemistry given the number of variables: a few simple laminar configurations
 - ❑ **Homogeneous systems (no transport terms)**
 - ❑ Isochoric adiabatic reactor
 - ❑ Isobaric adiabatic reactor
 - ❑ **One-dimensional systems**
 - ❑ Freely propagating laminar flame
 - ❑ Burner stabilized laminar flame
 - ❑ Counterflow diffusion flame
 - ❑ **Idealized reactors**
 - ❑ Partially stirred reactor: homogeneous at the macro level, heterogeneous at the micro level to mimic molecular diffusions when testing kinetic models

Far cry from actual turbulent configurations!

Numerical simulations

- ❑ Number of variables limit detailed numerical solutions to a few simple laminar configurations

Isochoric adiabatic reactor

► Governing Equations

$$\rho \frac{dY_j}{dt} = W_j \omega_j$$

$$\rho \left(c_p - \frac{R}{W} \right) \frac{dT}{dt} + \sum_{j=1}^n \left(h_j - \frac{R}{W_j} \right) W_j \omega_j = 0$$

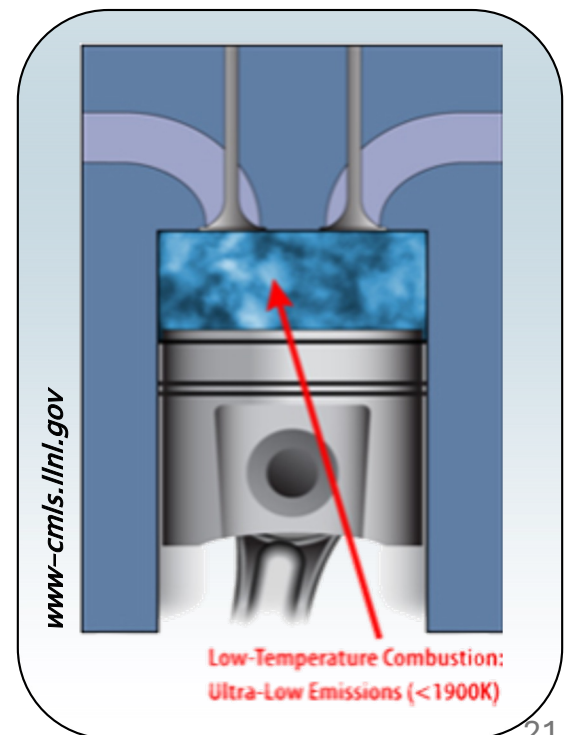
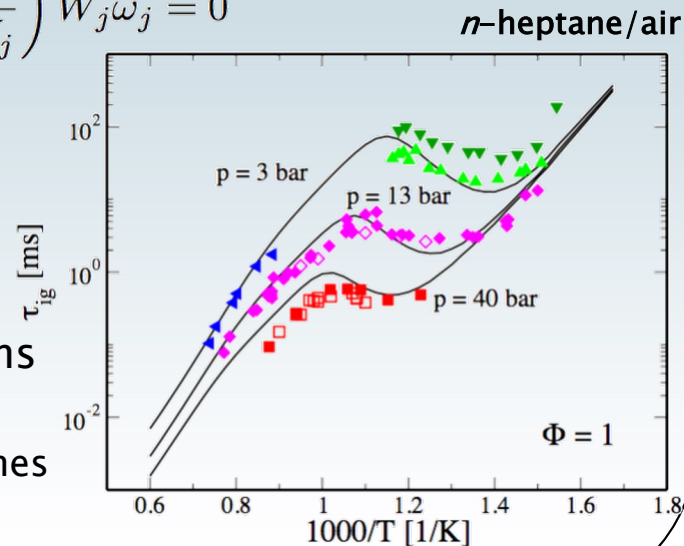
$$P = \frac{\rho RT}{W}$$

► Type of information

- Ignition delay time

► Experimental configurations

- Shock tube
- rapid compression machines



Numerical simulations

- ❑ Number of variables limit detailed numerical solutions to a few simple laminar configurations

Isobaric adiabatic reactor

► Governing Equations

$$\rho \frac{dY_j}{dt} = W_j \omega_j$$

$$\rho c_p \frac{dT}{dt} + \sum_{j=1}^n h_j W_j \omega_j = 0$$

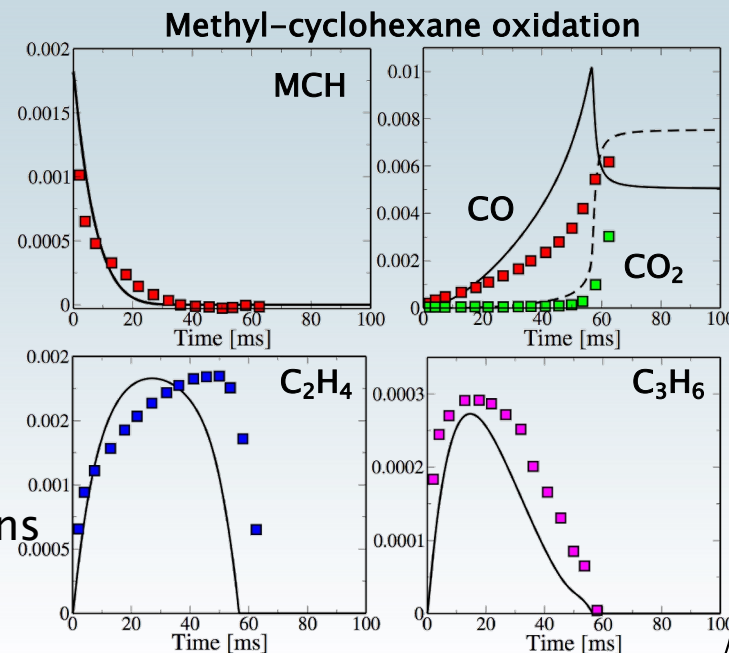
$$\rho = \frac{PW}{RT}$$

► Type of information

- species concentrations

► Experimental configurations

- Plug Flow Reactor (PFR)
- Diluted or lean mixtures



Numerical simulations

- ❑ Number of variables limit detailed numerical solutions to a few simple laminar configurations

Propagating laminar flame

▶ Governing Equations

$$\rho V = \text{const}$$

$$\rho V \frac{dY_j}{dy} + \frac{d}{dy} (\rho Y_j v_j) = W_j \omega_j$$

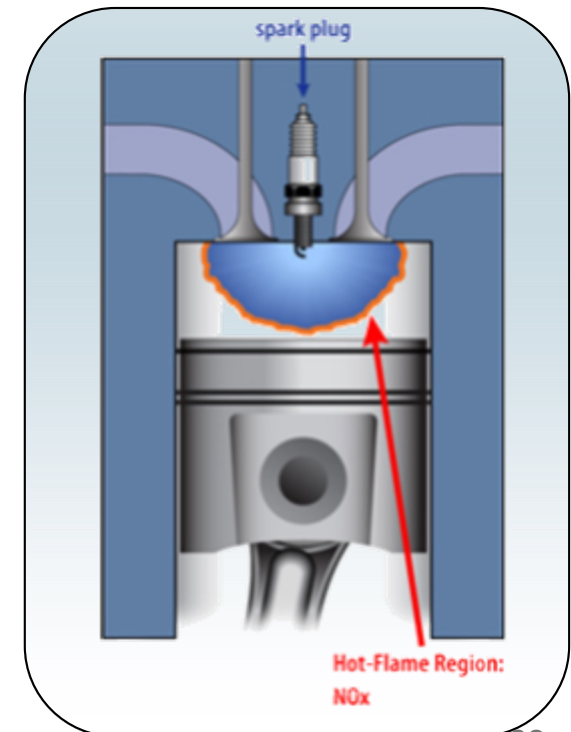
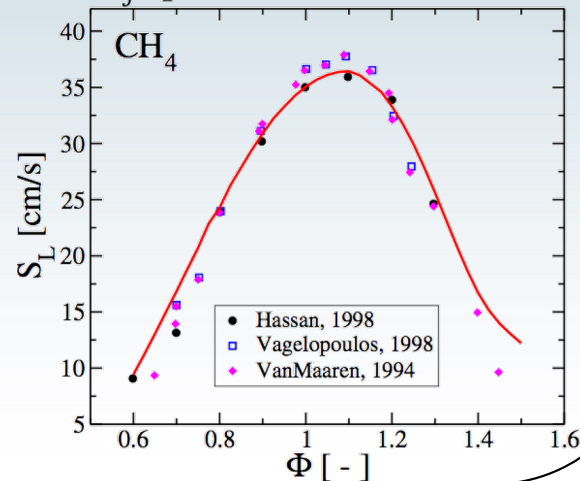
$$\rho V \frac{dT}{dy} - \frac{d}{dy} \left(\lambda \frac{dT}{dy} \right) + \frac{d}{dy} \left(\rho Y_j v_j C_{p_j} \frac{dT}{dy} \right) + \sum_{j=1}^n h_j W_j \omega_j = 0$$

▶ Type of information

- Laminar burning velocity

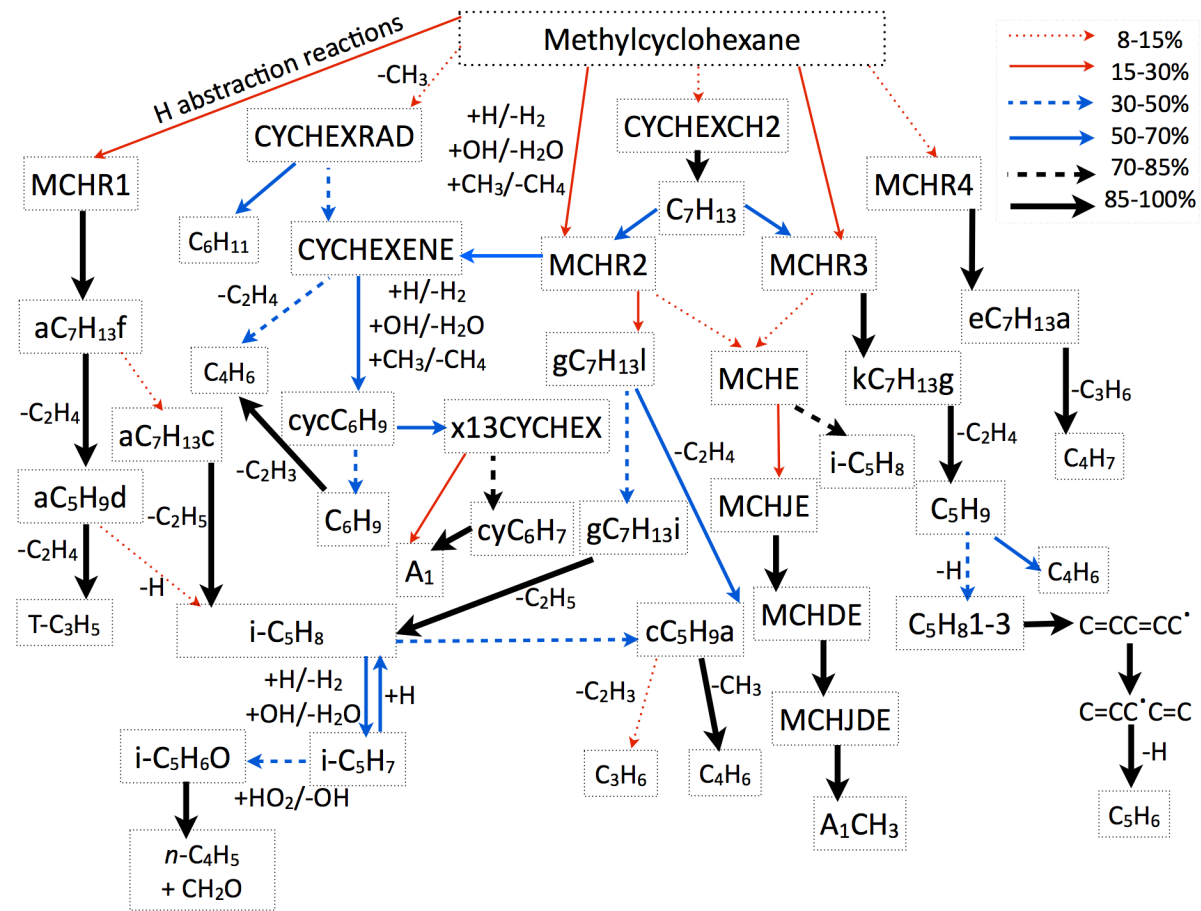
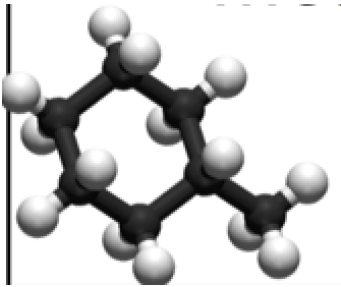
▶ Experimental configurations

- Combustion bomb



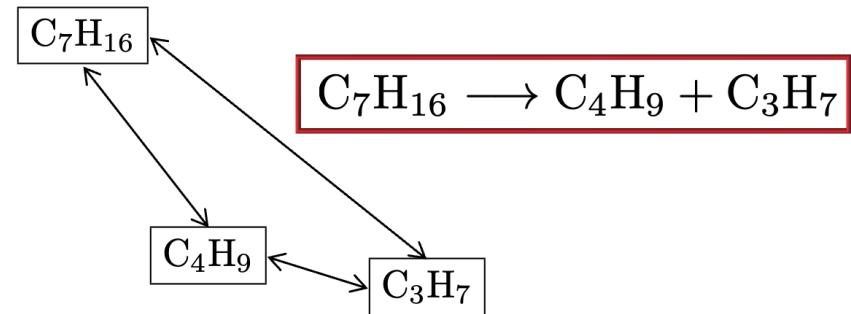
Chemical model reduction

- ❑ Chemical kinetic mechanism is a network, from which we want to extract the most important connections for some conditions of interest



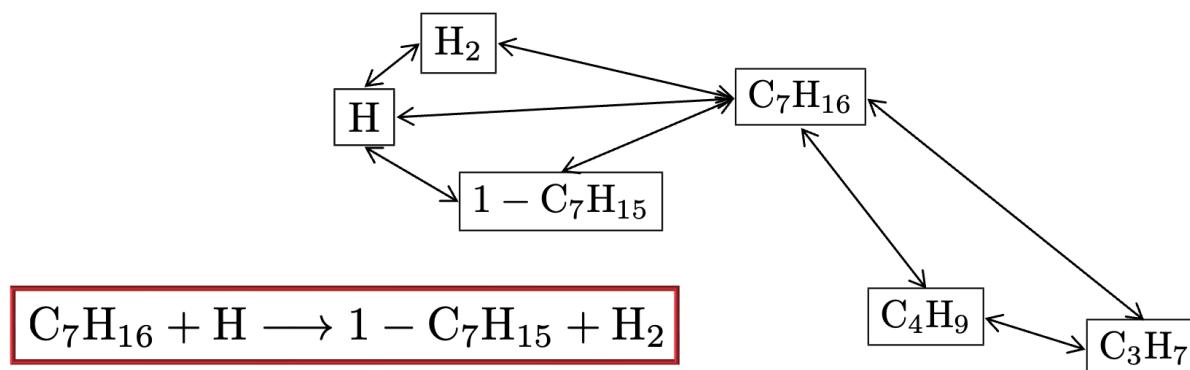
Chemical model reduction

- View reaction mechanism as kinetic network, well represented as a directed graph



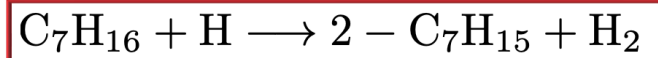
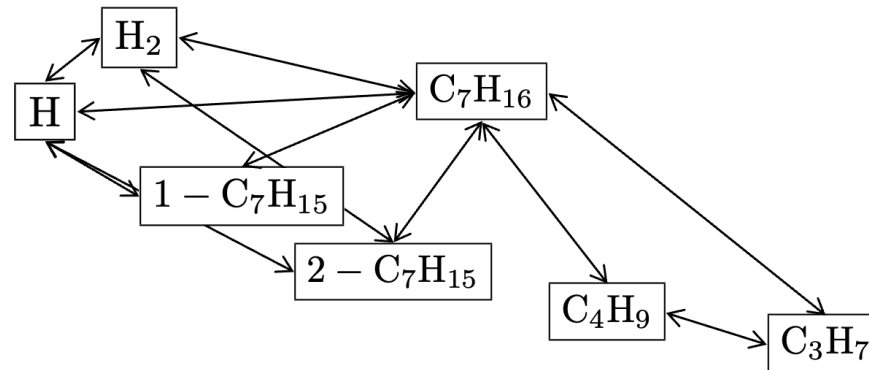
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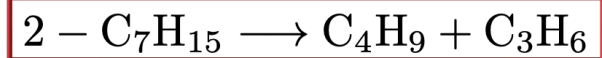
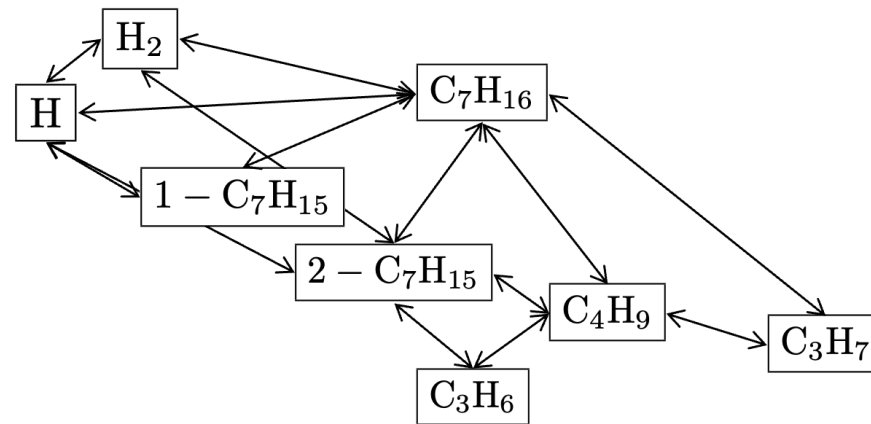
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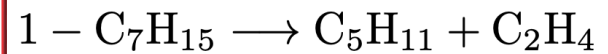
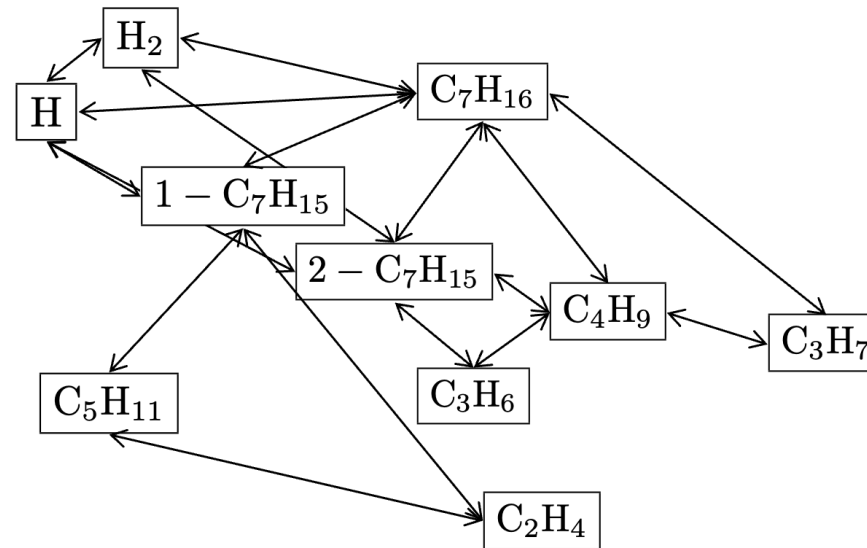
Chemical model reduction

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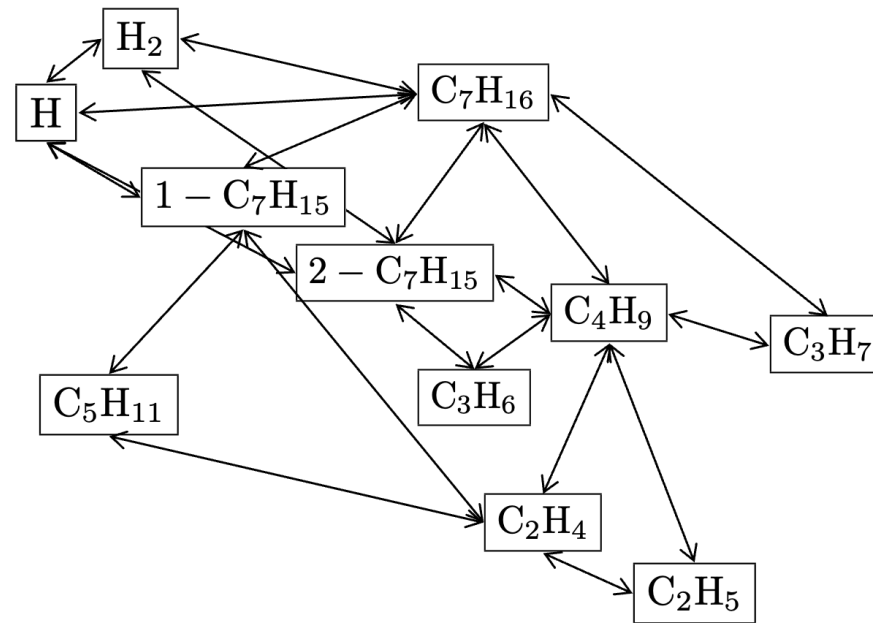
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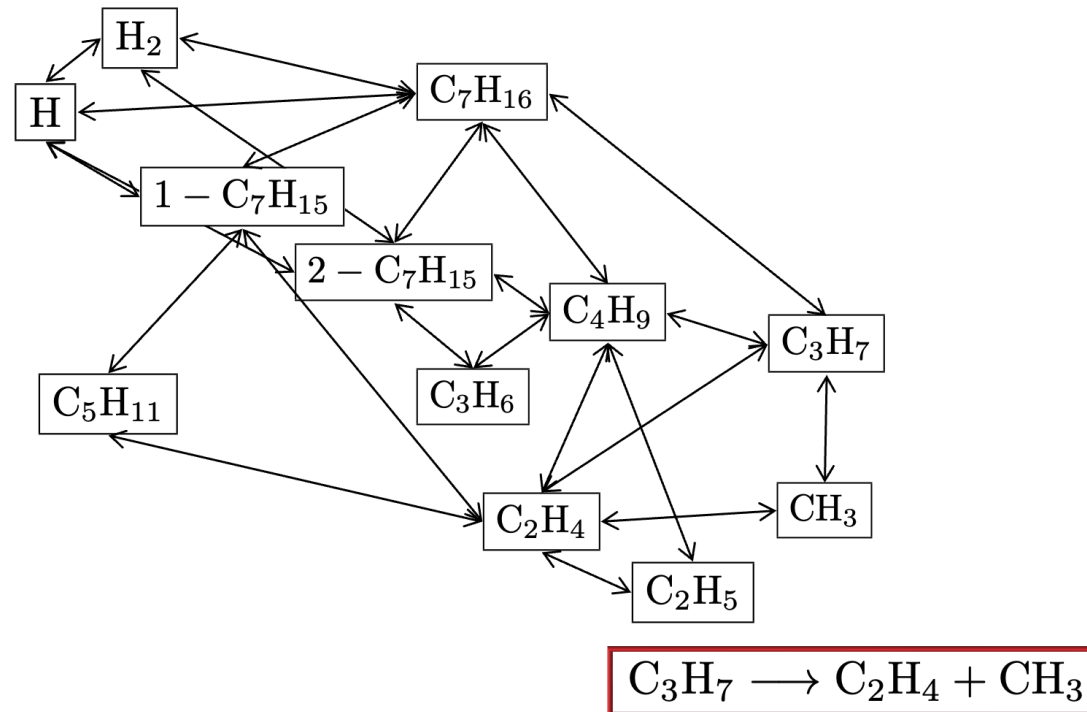
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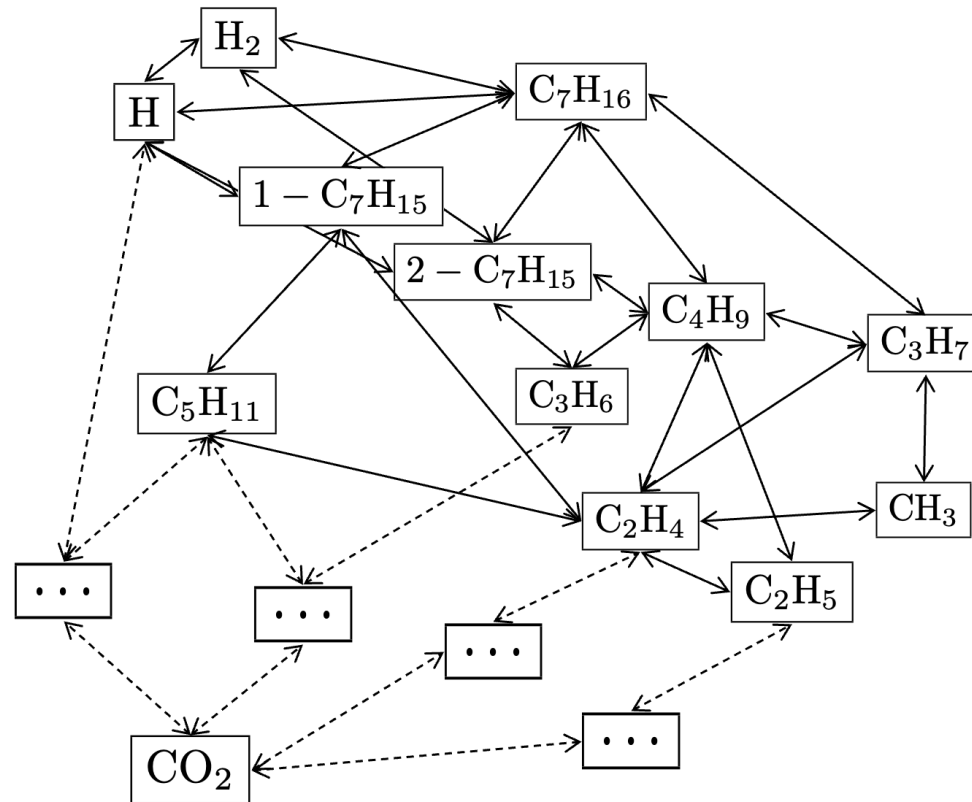
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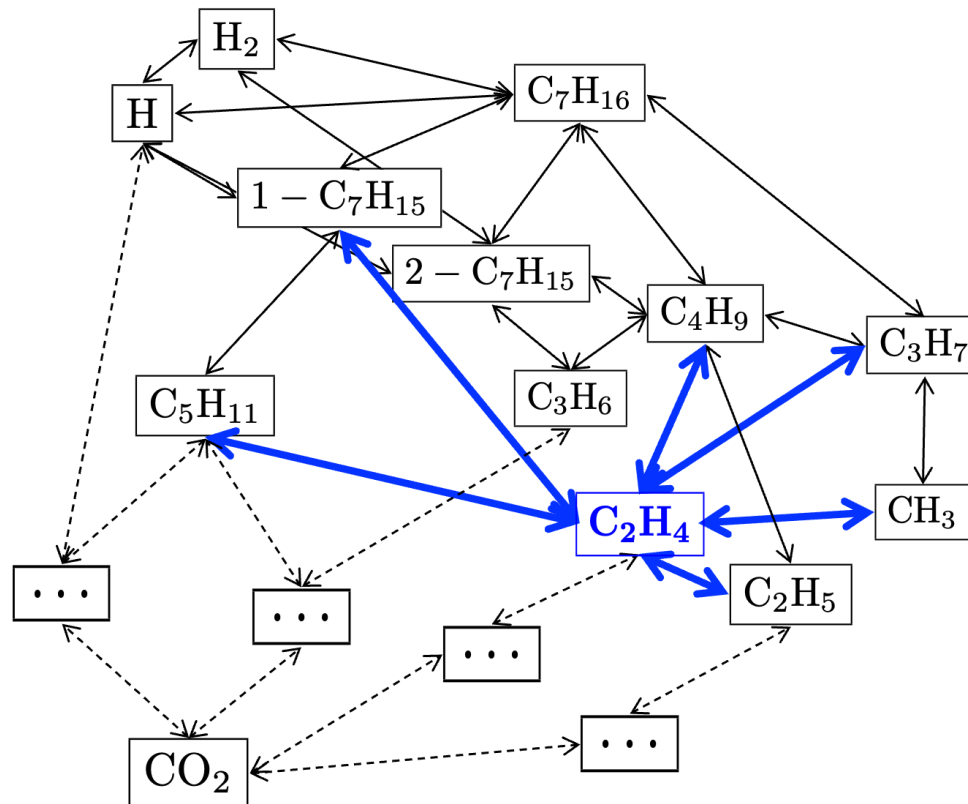
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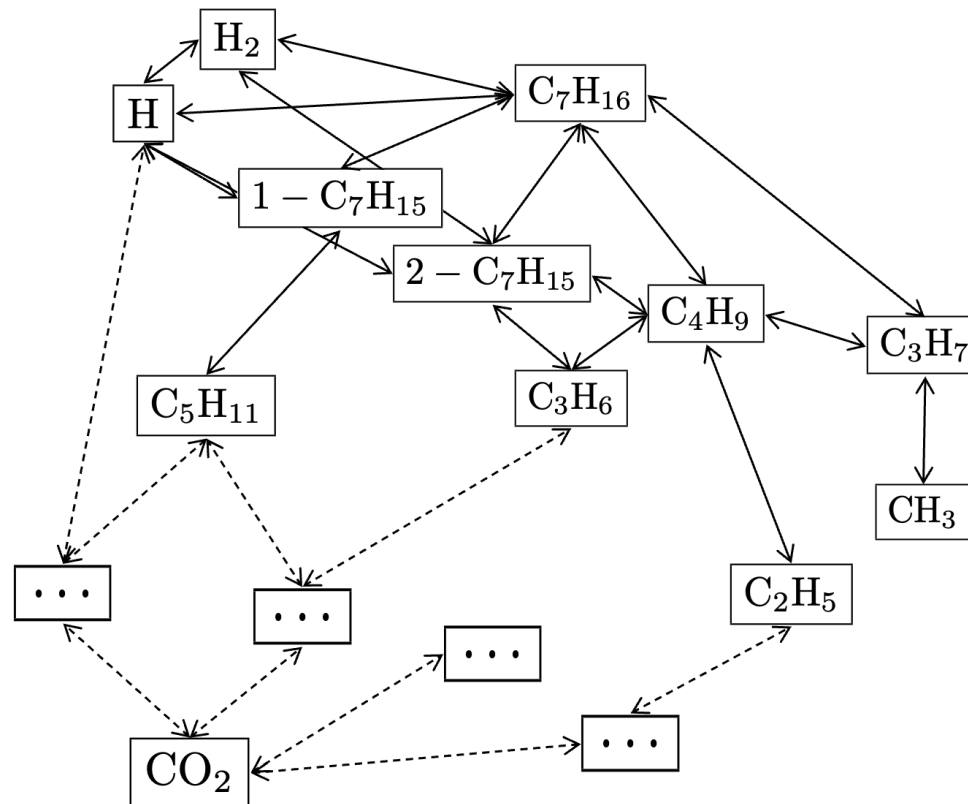
Directed Relation Graph family of techniques

- **Species reduction:** Identify nodes to remove, along with their connections



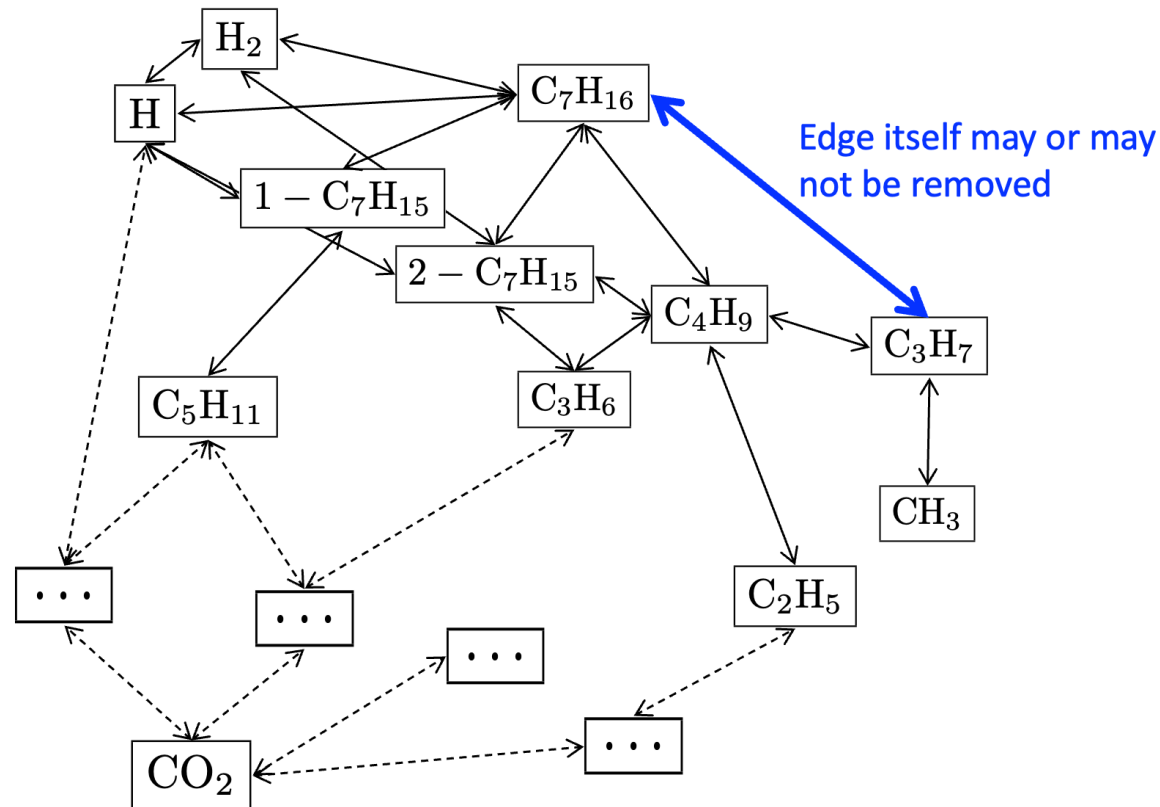
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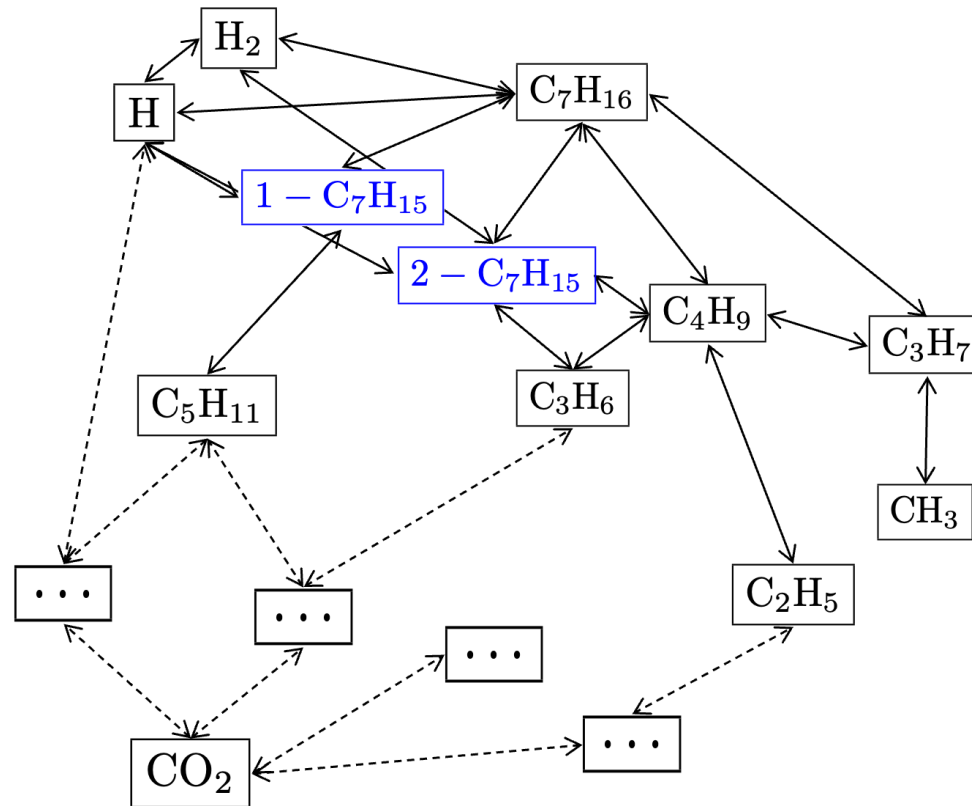
Directed Relation Graph family of techniques

- ❑ **Species reduction:** Identify nodes to remove, along with their connections
- ❑ **Reaction reduction:** Identify edge contributions to remove



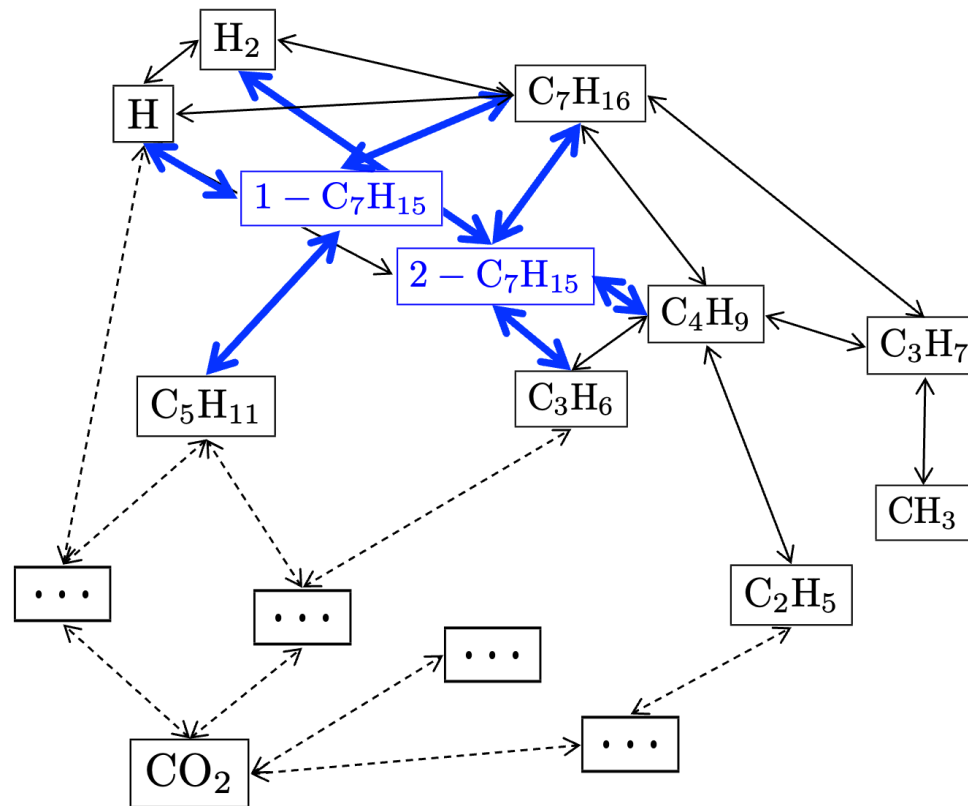
Directed Relation Graph family of techniques

- ❑ **Species reduction:** Identify nodes to remove, along with their connections
- ❑ **Reaction reduction:** Identify edge contributions to remove
- ❑ **Isomer Lumping:** Merge nodes



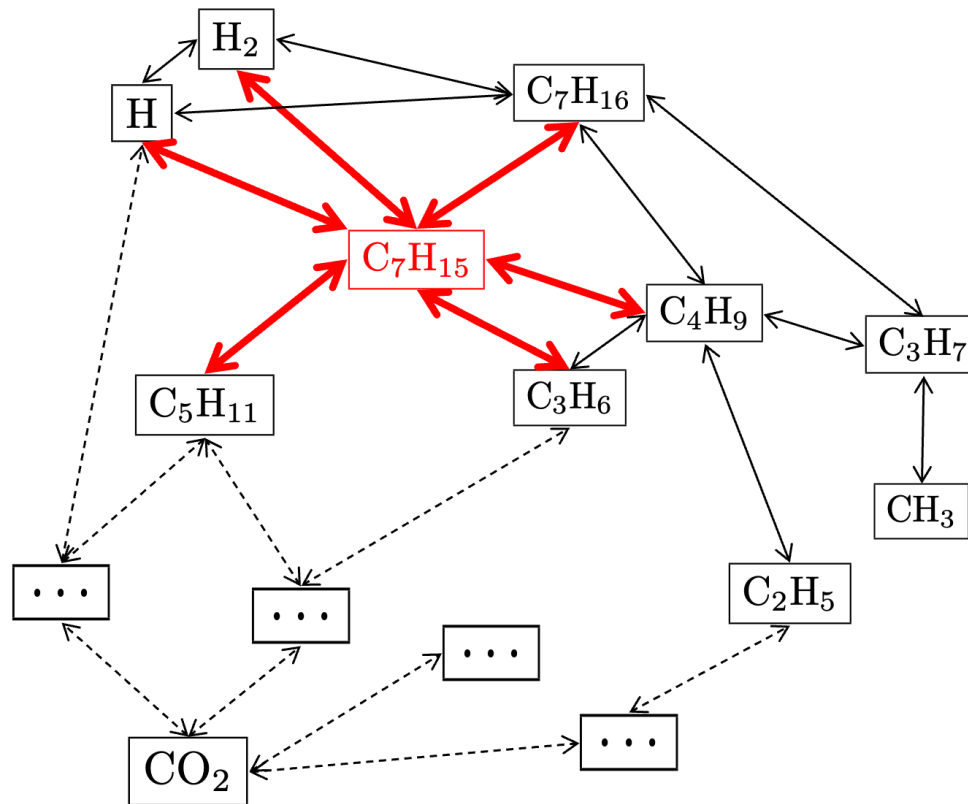
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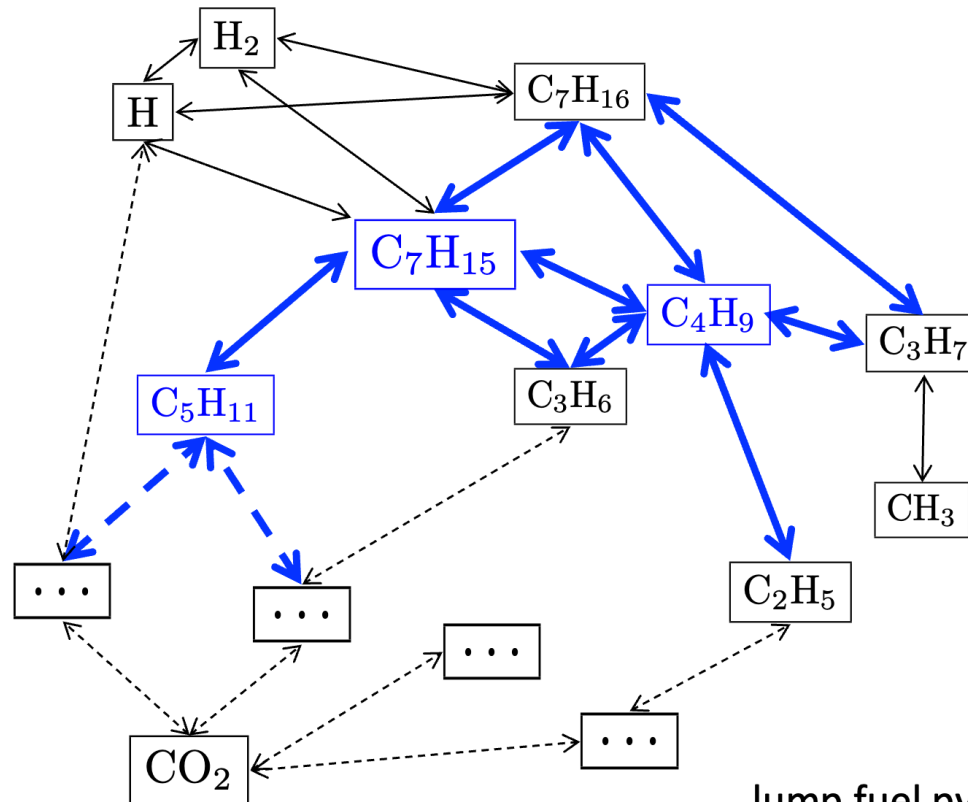
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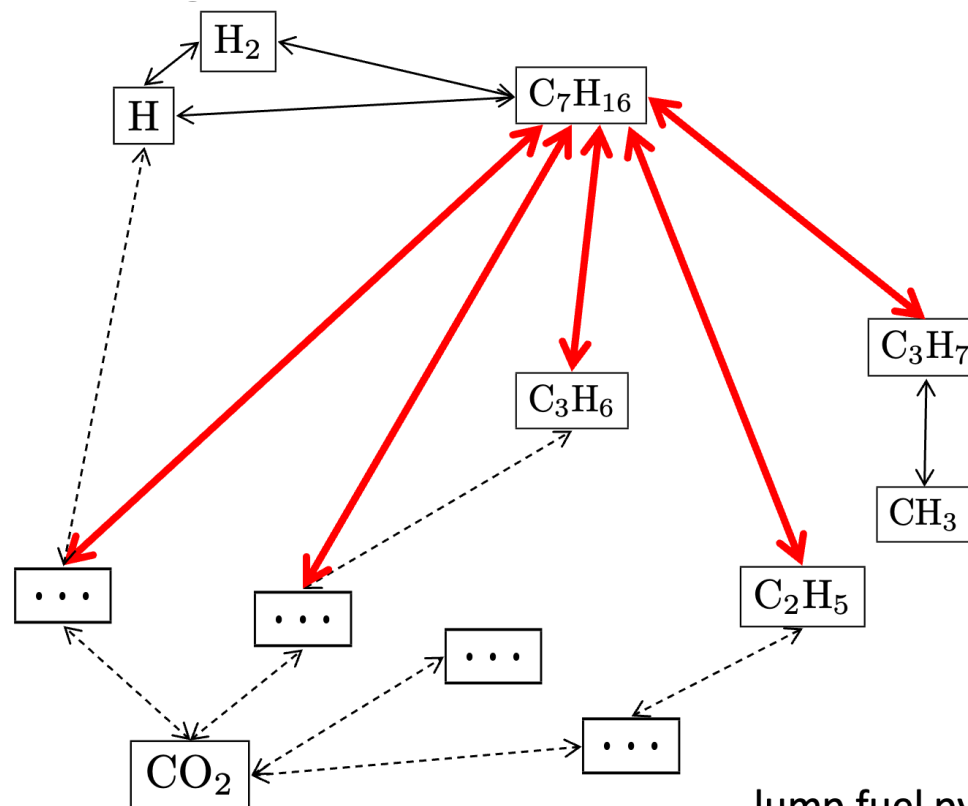
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- ❑ **Isomer Lumping:** Merge nodes
- ❑ **Path lumping:**
collapse entire sections of the network



Example:
lump fuel pyrolysis pathway up to C3

Directed Relation Graph family of techniques

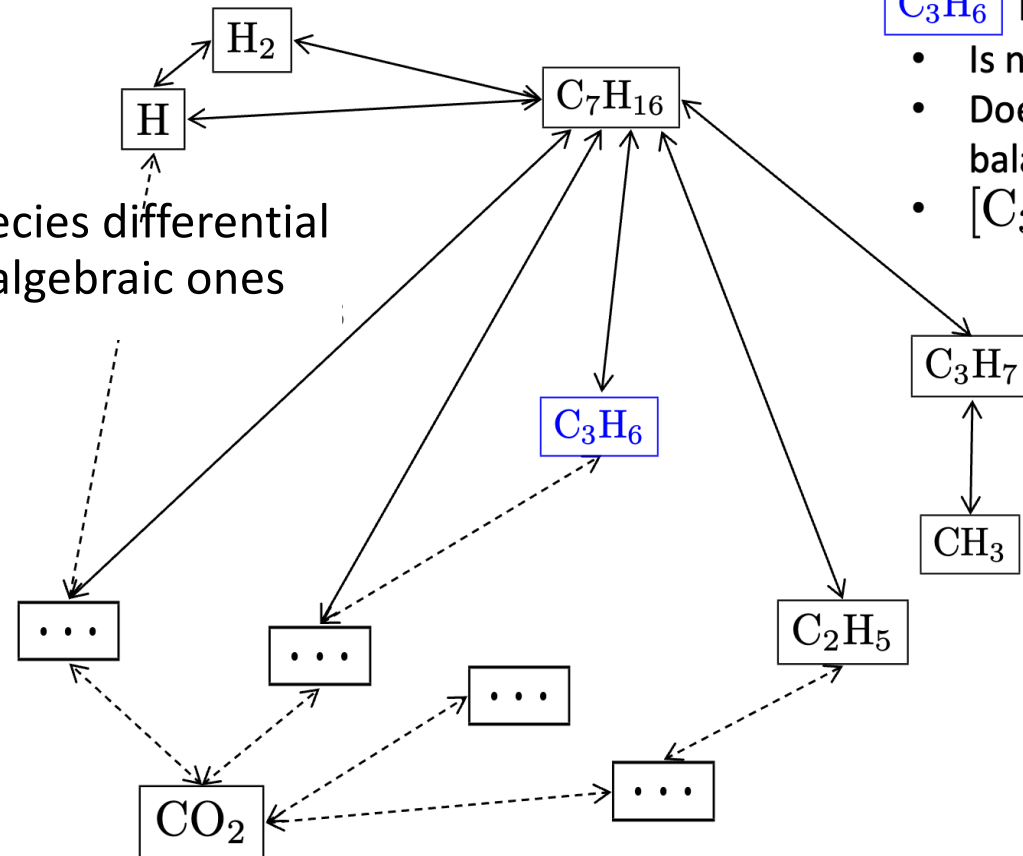
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- ❑ **Path lumping:** collapse entire sections of the network
- ❑ **QSS:** replace species differential equations with algebraic ones

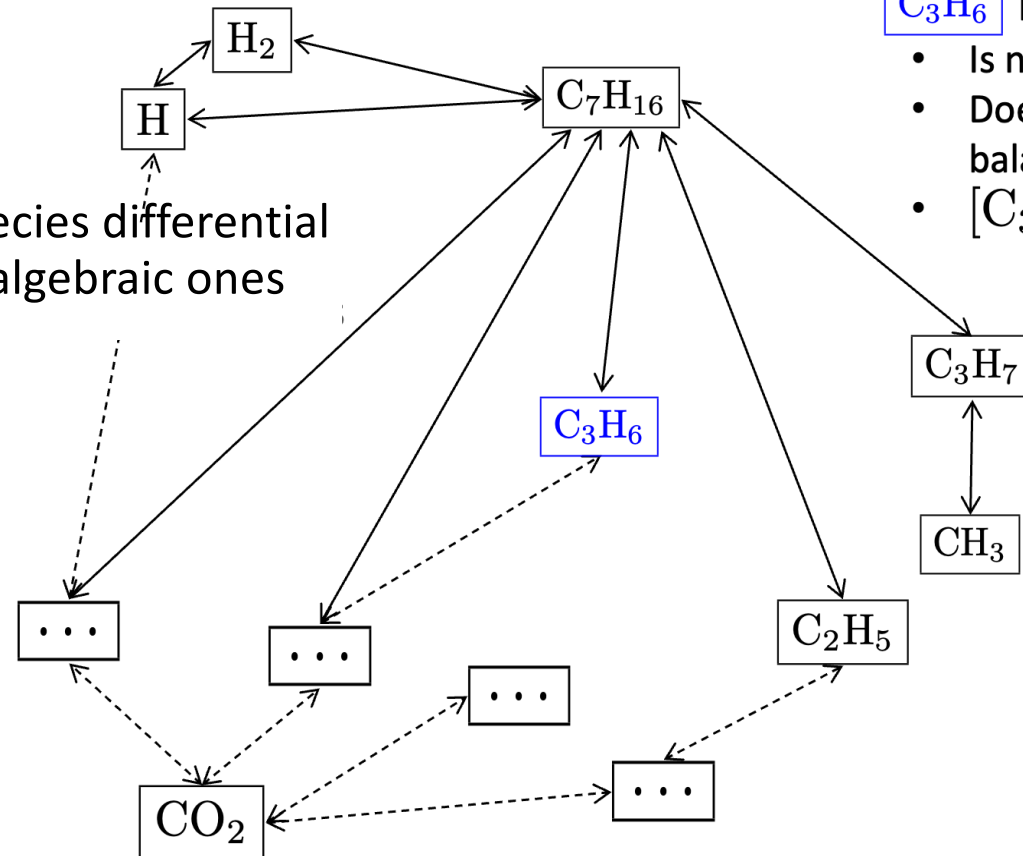


C_3H_6 becomes a fictitious species

- Is not transported
- Does not contribute to mass balance
- $[C_3H_6] = f([S_i]_{i \notin \text{QSS}})$

Directed Relation Graph family of techniques

- ❑ **Species reduction:** Identify nodes to remove, along with their connections
- ❑ **Reaction reduction:** Identify edge contributions to remove
- ❑ **Isomer Lumping:** Merge nodes
- ❑ **Path lumping:** collapse entire sections of the network
- ❑ **QSS:** replace species differential equations with algebraic ones
- ❑ **Projection/ML** techniques

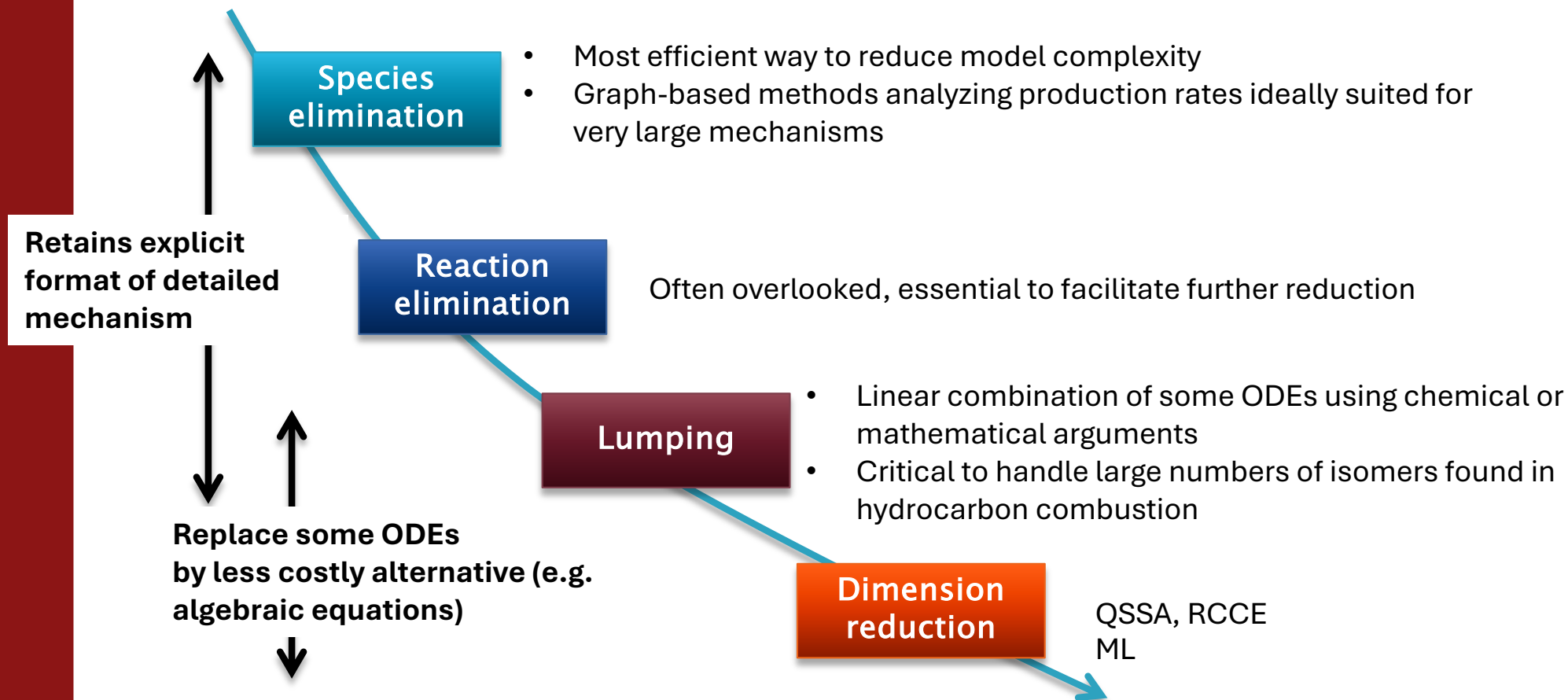


C₃H₆ becomes a fictitious species

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Chemical model reduction

- **Objective:** simplify the coupled set of ODEs describing the temporal evolution of a spatially homogeneous mixture of chemical species or simple 1D flames



Example – Jet fuel surrogate

	Jet-A (POSF 4658)	Jet Fuel Surrogate
Formula	$C_{10.2}H_{19.9}$	$C_{9.4}H_{18.4}$
Molecular weight [g/mol]	142±5	131
H/C ratio	1.957	1.95
CN	47.1±0.3	56.5
TSI	21.4	14.1
Composition (vol %)		
Aromatics	20%	15.8% m-Xylene
Paraffins	60%	58.5% n-Dodecane
Napthalenes	20%	25.7% methyl-cyclohexane

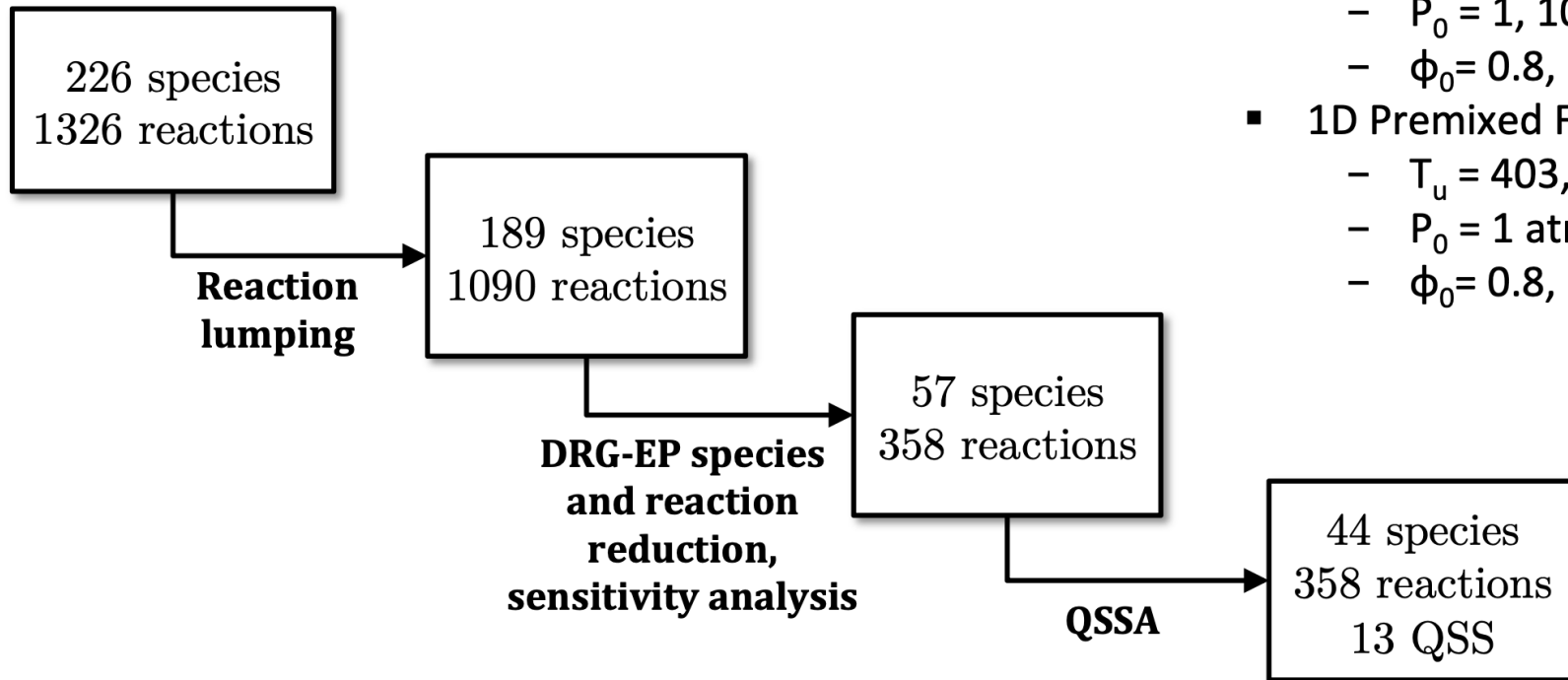
Chosen based on mechanism availability, component classes in jet fuel

Initial composition formulated to match H/C, CN, TSI, MW

Final composition optimized against Jet-A flame speeds and ignition delay times

Example – Jet fuel surrogate

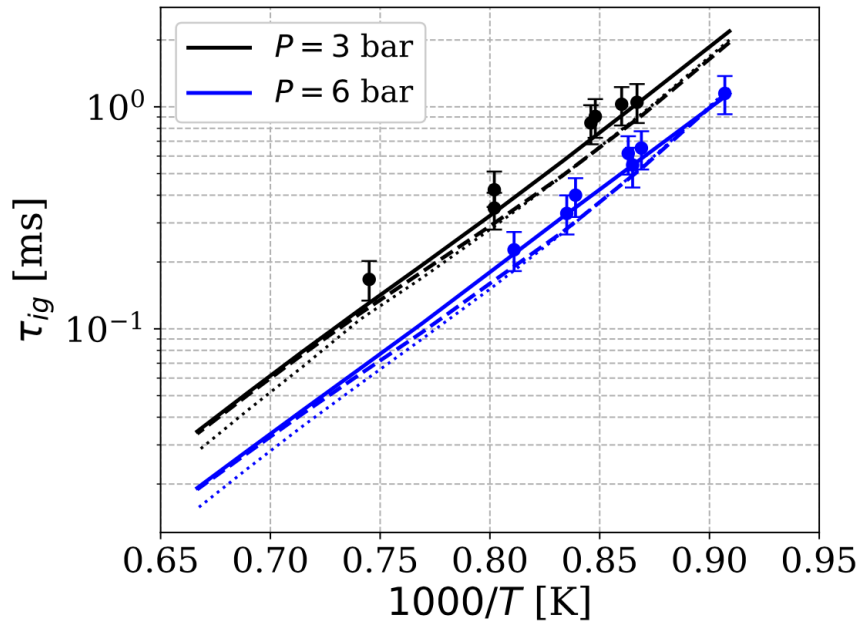
Detailed Mechanism



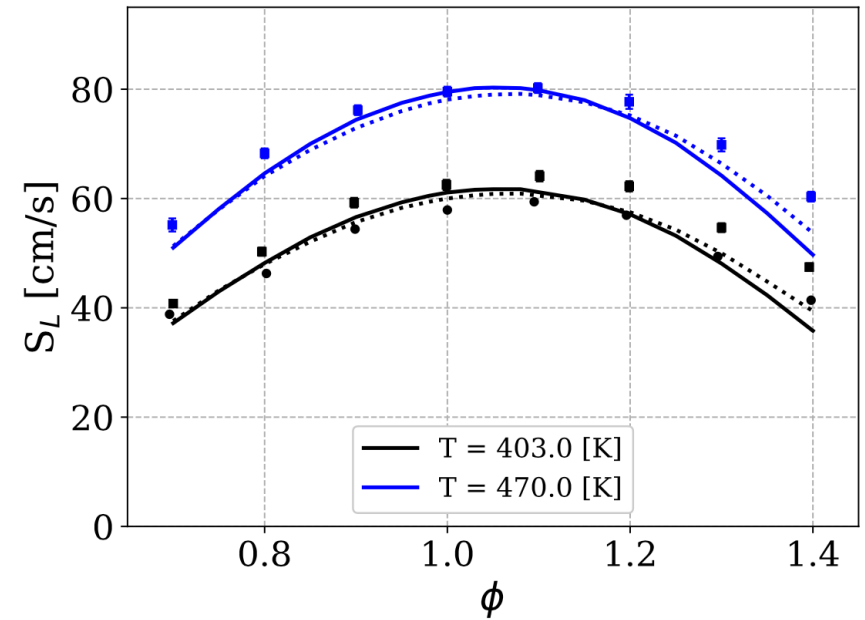
Reduction cases

- 0D Isochor Auto-Ignition
 - $T_0 = 1100, 1300, 1600\text{K}$
 - $P_0 = 1, 10\text{ atm}$
 - $\phi_0 = 0.8, 1, 1.3$
- 1D Premixed Flame
 - $T_u = 403, 470\text{K}$
 - $P_0 = 1\text{ atm}$
 - $\phi_0 = 0.8, 1, 1.3$

Example – Jet fuel surrogate



Ignition delay times in an isochor reactor at $\phi_0 = 1$ compared to experimental results with Jet-A^{1,2,3}.



Laminar flame speeds at atmospheric pressure compared to experimental results with Jet-A^{1,2}.

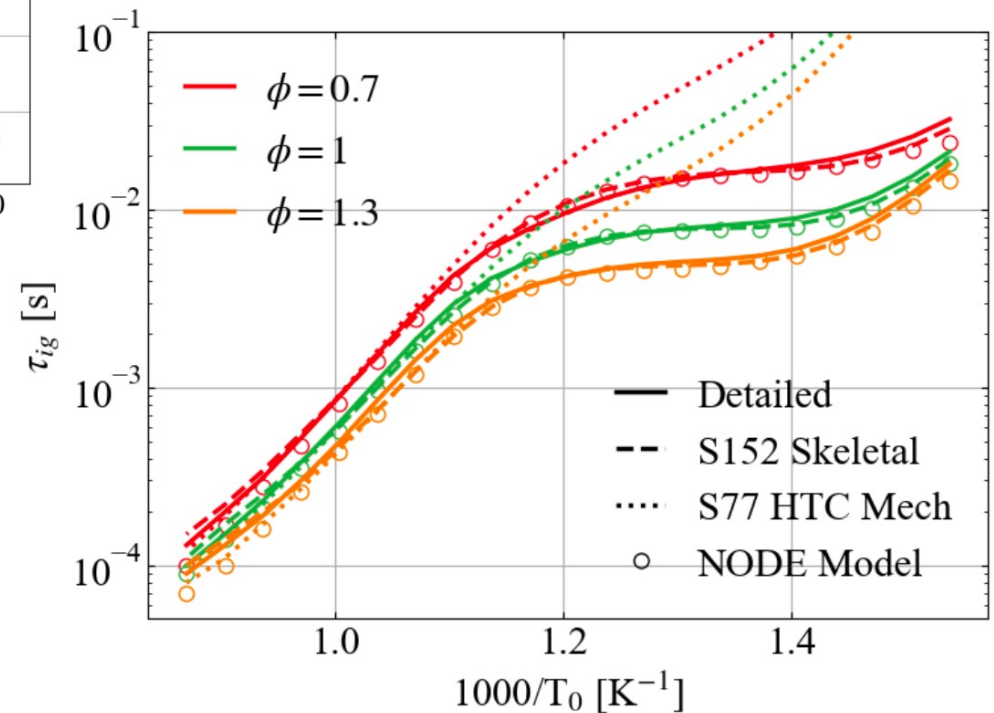
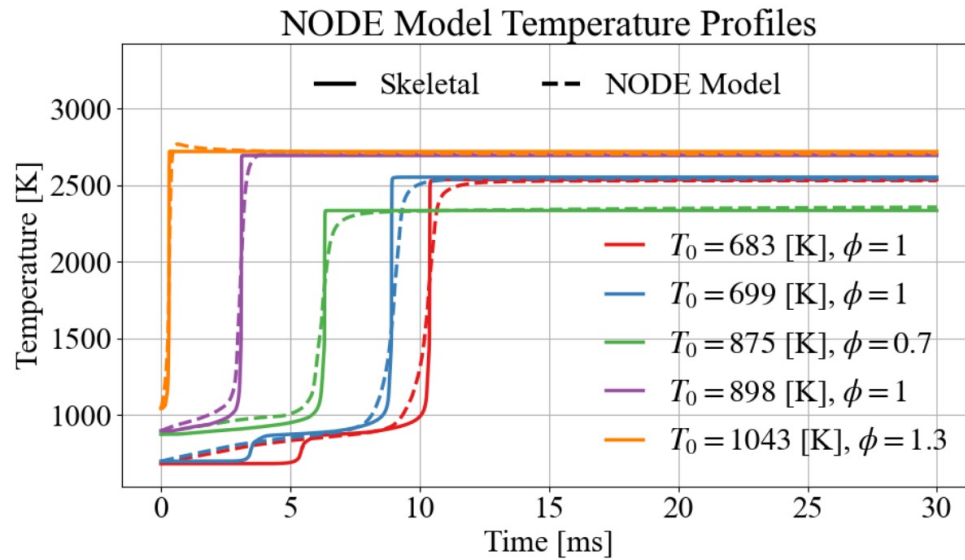
■ ● = experiments
 — = detailed,
 - - = lumped,
 - - - - = 44 species QSS

¹Zhu, Y. et al. *Proc. Combust. Inst.* 2015.

²Dean, A. et al. *Proc. Combust. Inst.* 2007.

³Wang, H. et al. *Fuel*. 2012.

Example with ML – SAF



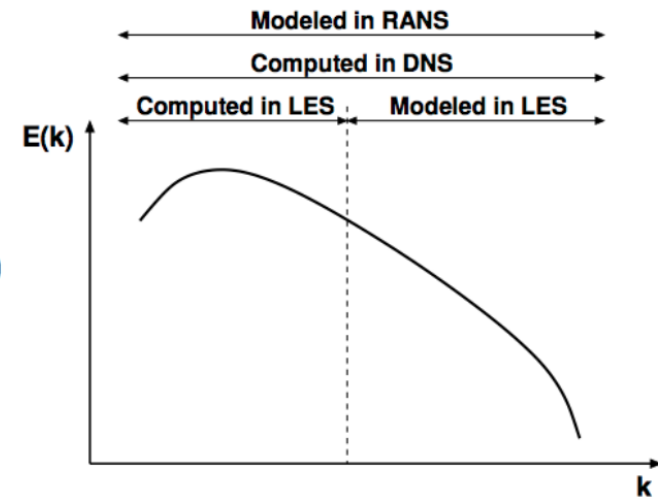
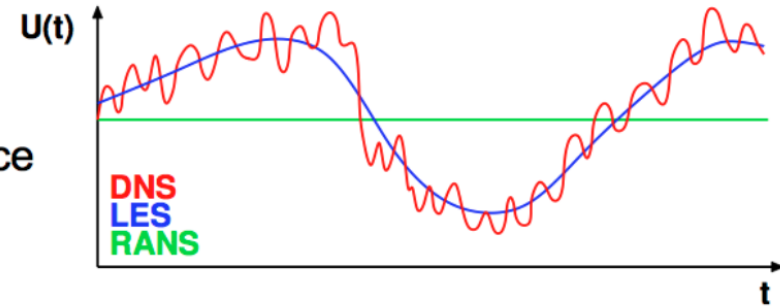
Ignition delay time well predicted with only 6 latent variables over a wide range of conditions compared to 152 species using the state-of-the-art skeletal reduction technique

Chemical kinetics and CFD simulation of turbulent combustion

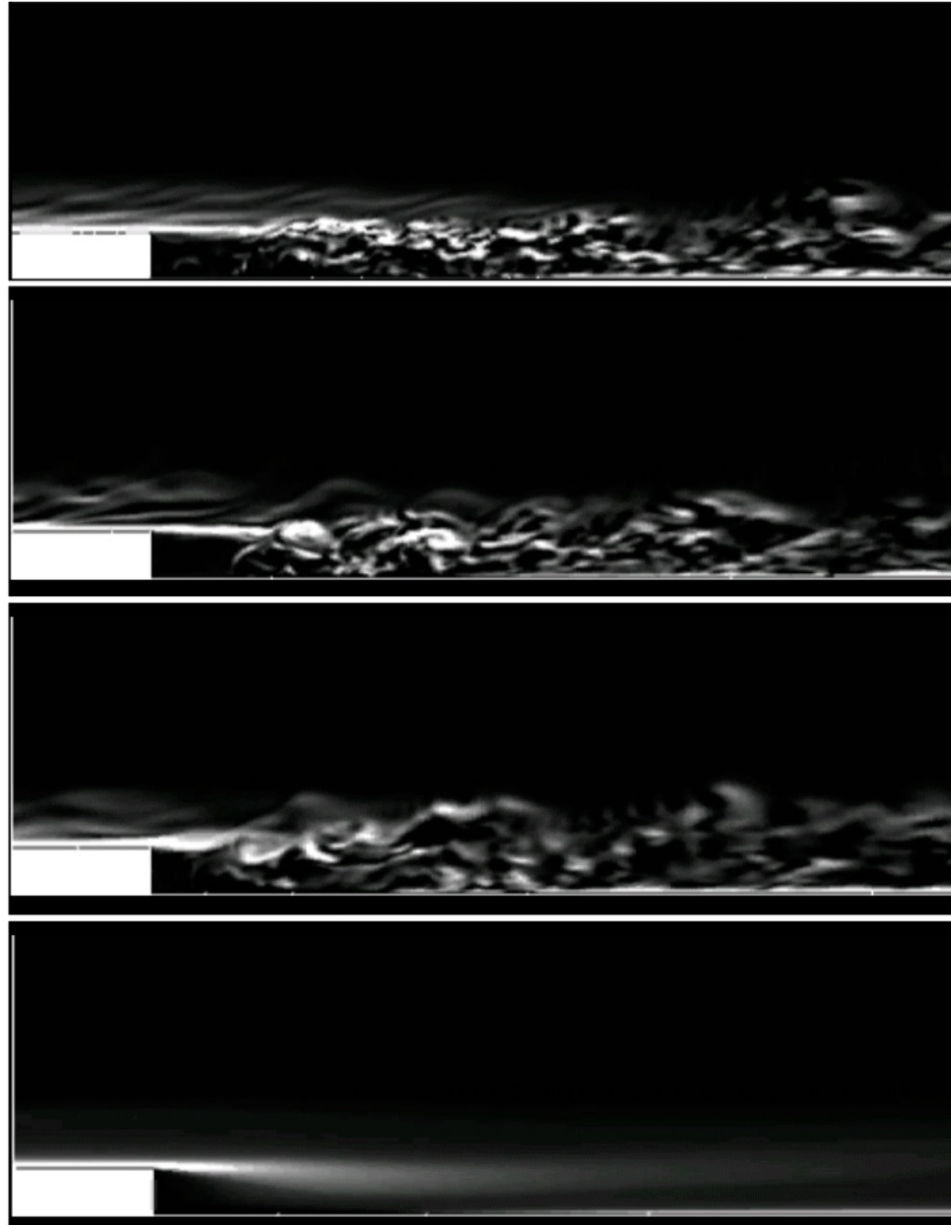
A good model is the **simplest model** that contains the physics we care about

Numerical frameworks to simulate turbulence

- Direct Numerical Simulation (DNS)
 - Resolve all flow scales directly
 - No need for physical model of turbulence
 - Very high cost
- Large Eddy Simulation (LES)
 - Resolve large flow scales
 - Model small scales only
 - Moderate cost
- Reynolds Averaged Navier-Stokes (RANS)
 - Solve for mean flow
 - Model all fluctuations
 - Low cost



Numerical frameworks to simulate turbulence

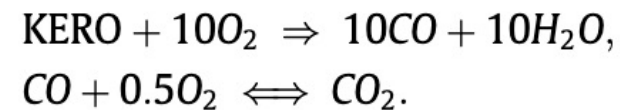


The issue of LES for turbulent combustion

- ❑ In LES, the Navier-Stokes equations are filtered: only the larger scales of the flow are resolved on the mesh
 - ❑ Works great for non-reactive turbulence because in many cases, what happens at the small scales is universal
 - ❑ But combustion usually happens at the small scales, and it is definitely not universal (e.g. premixed vs non-premixed)
- ❑ Very large body of work to develop models to “close” the governing equations and properly account for the effect of the combustion (small scale) on the filtered quantities (large scale)
 - ❑ Strong simplification assumption: e.g. eddy dissipation model
 - ❑ Conditional moment closure models:
 - ❑ Tabulation-based – e.g. FPV, FGM, FPI
 - ❑ Monte-Carlo based
 - ❑ Thickened flame models
 - ❑ ...

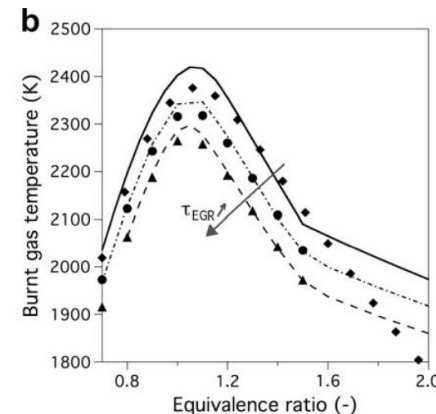
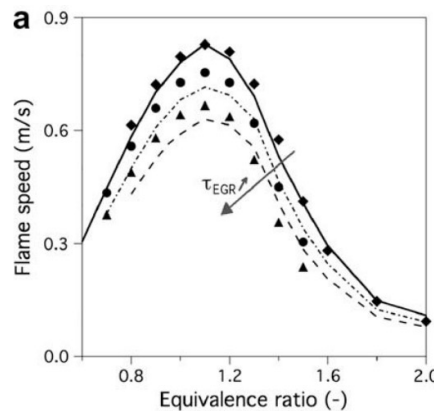
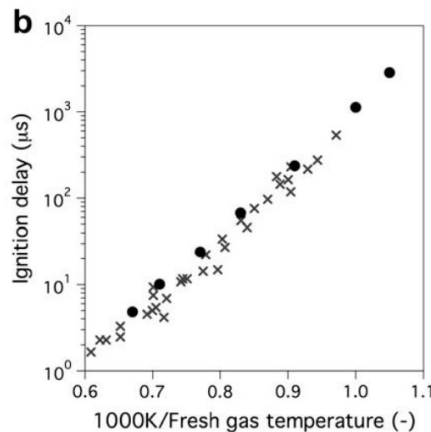
Not all simulations need the details of the chemistry!

- ❑ In many industrial applications, only a few species are of interest and taking into account a large set of species is usually not needed.
- ❑ Example: In gas turbines, a large part of the design process may just need :
 - ❑ The chamber efficiency (which requires a correct prediction of fuel reaction rates),
 - ❑ The outlet temperature (which requires correct equilibrium computations)
 - ❑ CO composition at the chamber exit
- ❑ 2 or 3 step models are able to do that.
 - ❑ Ex: 2S_KERO_BFE 2 steps model
 - ❑ Parameters fitted to capture flame speed, burnt gas temperature and ignition delays at relevant conditions
 - ❑ Fuel can be changed



$$k_{f,1} = A_1 f_1(\phi) e^{(-E_{a,1}/RT)} [\text{KERO}]^{n_{\text{KERO}}} [\text{O}_2]^{n_{\text{O}_2,1}},$$

$$k_{f,2} = A_2 f_2(\phi) e^{(-E_{a,2}/RT)} [\text{CO}]^{n_{\text{CO}}} [\text{O}_2]^{n_{\text{O}_2,2}},$$



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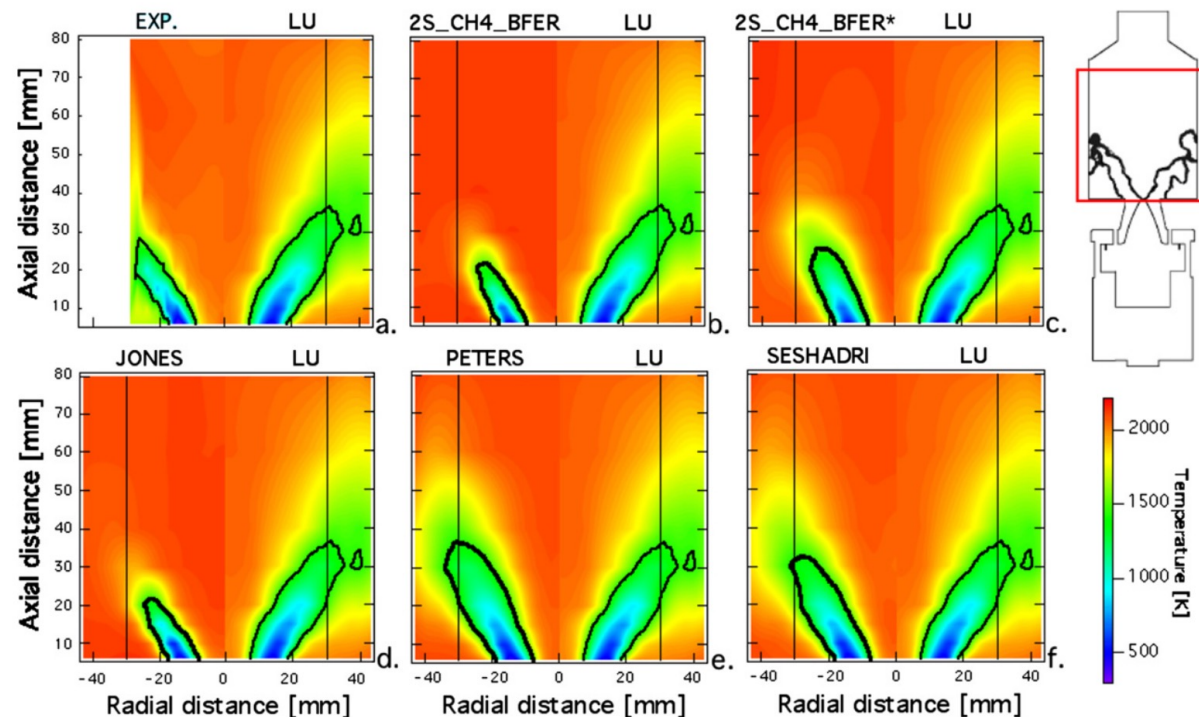


Fig. 5. Mean temperature field in the vertical mid-plane. (a) Comparison between experiments and LU scheme. (b)–(f) Comparison between reduced schemes and reference LU mechanism. The black isoline of progress variable $c = 0.65$ represents the mean flame surface position.